# The reactivity of 'stored NH<sub>3</sub>' with NO on V<sub>2</sub>O<sub>5</sub>/TiO<sub>2</sub> catalyst in NH<sub>3</sub>-SCR (Selective catalytic reduction) at low temperature

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**Abstract:** In this study, transient experiments were carried out to investigate the reactivity of stored  $NH_3$  in ' $NH_3$  reservoir', or chemisorbed  $NH_3$  on  $V_2O_5/TiO_2$  catalyst, with gas phase NO in lean conditions at low temperatures. DFT calculation was used to compare the reaction pathways between  $NH_3$  adsorbed on Brønsted acid site and that on Lewis acid site.

Keywords: Selective catalytic reduction, vanadia, V2O5/TiO2, transient experiment, chemisorbed NH3.

# **1. Introduction**

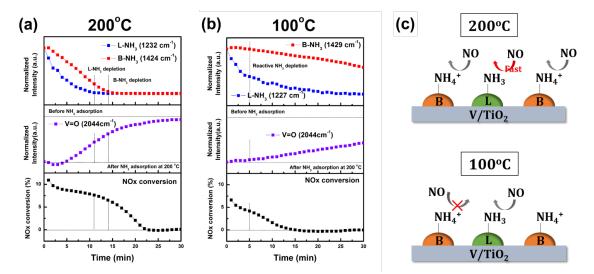
Selective catalytic reduction (SCR) using  $V_2O_5/TiO_2$  catalysts is the state-of-the-art technology to remove  $NO_x$  from emission for stationary and mobile sources. Although many researches have been performed to investigate the structure-activity relationships of vanadium-based catalyst in SCR reaction, few works were reported regarding the correlation between the acidic properties of dispersed vanadium oxide species and its SCR performance. It has been suggested before that acid sites on catalysts can act as an 'NH<sub>3</sub> reservoir' during SCR reaction, which means that the catalyst can remove  $NO_x$  for a few minutes even after stopping the NH<sub>3</sub> supply.<sup>1,2</sup> The surface of catalyst was monitored by in situ DRIFT to track the state of adsorbed NH<sub>3</sub> species while checking outlet gas with NOx analyzer to measure catalytic activity simultaneously.

#### 2. Experimental

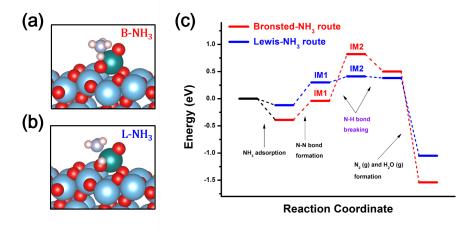
In this experiment,  $V_2O_5/TiO_2$  catalyst was prepared by conventional wet impregnation method using microporous TiO<sub>2</sub> with high surface area (251 m<sup>2</sup>/g) as a support material.<sup>3</sup> *In situ* DRIFT spectra were obtained with FT-IR spectroscopy (Nicolet 6700, Thermo Scientific) equipped with high-temperature DRIFT cell fitted with ZnSe windows. Catalysts were saturated with 0.38 Torr of NH<sub>3</sub> at 100 °C and 200 °C, and subsequently reacted with NO and O<sub>2</sub> flow. During reaction, NO and NO<sub>2</sub> concentration were also monitored using NO<sub>x</sub> chemiluminescence analyzer (42i High level, Thermo Scientific). The periodic density functional theory (DFT) calculations were performed with a Vienna ab initio simulation package (VASP). A slab model of anatase TiO<sub>2</sub>(101) surface was used in this work (10.38 × 7.65 Å<sup>2</sup>), which has a (1 × 2) surface unit cell with four stoichiometric TiO<sub>2</sub> layers and a vacuum spacing of 15 Å.

# 3. Results and discussion

The experiment at 200 °C showed that SCR activity gradually slowed down with the depletion of NH<sub>3</sub> adsorbed on Lewis acid site (L-NH<sub>3</sub>) and that on Brønsted acid site (B-NH<sub>3</sub>) as shown in Figure 1(a). In contrast, the experiment at 100 °C (Figure 1(b)) showed that the reaction stopped after the depletion of L-NH<sub>3</sub>, even in the presence of the stored B-NH<sub>3</sub>. This implies that B-NH<sub>3</sub> cannot act as an NH<sub>3</sub> reservoir at low temperature like 100 °C, which limits the number of participating NH<sub>3</sub> on the catalyst surface. With increasing temperature from 100 to 200 °C, we observe the migration of residual NH<sub>3</sub> between different acid sites. Thus, NO reduction with stored NH<sub>3</sub> on V<sub>2</sub>O<sub>5</sub>/TiO<sub>2</sub> catalyst occurred more dominantly on Lewis acid site, while the participation of B-NH<sub>3</sub> in SCR reaction was found to be more temperature-dependent than L-NH<sub>3</sub>, as illustrated in Figure 1(c).



**Figure 1.** The reaction of adsorbed NH<sub>3</sub> with NO + O<sub>2</sub> feed was monitored with in situ DRIFT and NO<sub>x</sub> analyzer at (a) 200 °C and (b) 100 °C. (c) Schematic illustration of the different reactivity of stored NH<sub>3</sub> on V<sub>2</sub>O<sub>5</sub>/TiO<sub>2</sub> catalyst.



**Figure 2.** The optimized geometry of (a) NH<sub>4</sub><sup>+</sup> adsorbed on Brønsted acid site and (b) NH<sub>3</sub> on Lewis acid site. (c) Energy profile for NO reacting with Brønsted-NH<sub>3</sub> (red) and Lewis-NH<sub>3</sub> (blue), respectively.

Also, the reaction pathways of NO (g) with the adsorbed  $NH_3$  on catalyst surface, which is known as Eley-Rideal mechanism, were simulated by DFT calculation. Monomeric vanadium oxide on anatase  $TiO_2(101)$  surface was selected as a model system. In Figure 2(a) and Figure 2(b), the most stable positions of  $NH_3$  on Brønsted acid site and Lewis acid site were suggested, respectively. In the reaction with NO as shown in Figure 2(c), it was found that the Brønsted- $NH_3$  route is energetically less favorable than the Lewis- $NH_3$  route, which was consistent with the experimental results.

# 4. Conclusions

The reactivity of 'stored  $NH_3$ ' on  $V_2O_5/TiO_2$  was found to be strongly dependent on the type of acid sites. It was observed that  $NH_3$  adsorbed on Brønsted acid site was difficult to participate in SCR reaction especially at low temperature. DFT calculation results also confirmed that Lewis- $NH_3$  route is energetically more favorable than Brønsted- $NH_3$  route.

# References

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